**Experiment No#7**

**Objective:**

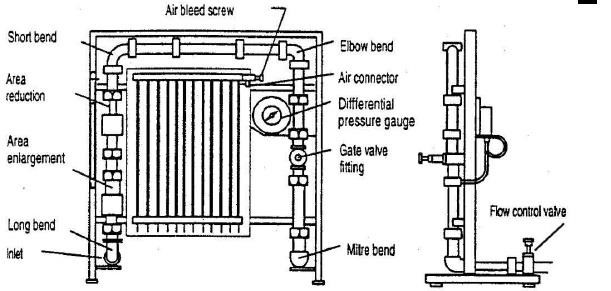
To calculate the energy losses in bends and pipe fittings.

**Theory:**

**Introduction**

Energy losses in pipe flows are the result of friction between the fluid and the pipe walls and internal friction between fluid particles.

Minor (secondary) head losses occur at any location in a pipe system where streamlines are not straight! such as at pipe junctions, bends, valves, contractions, expansions and reservoir inlets and outlets. In this experiment! you will measure minor head losses through a pipe section that has several bends, transitions! and fittings as shown in figure



The energy balance between two points in a pipe can be described by the Bernoulli equation, given by,

𝑝1 𝑉12 𝑝2 𝑉22

+𝑧1 + = +𝑧2 ++ℎ𝐿

𝛾 2𝑔 𝛾 2𝑔

where pi is static pressure (in Pa), at point i, γ is specific weight of the fluid (in N/m3), zi is the elevation (in meters), of point i, Vi is the fluid velocity (in m/s), at point i, g is the gravitational constant (in m/s2), and hL is head loss (in meters), The term 𝑝𝑖 is referred to as the static head; zi is the elevation head; and

𝛾

𝑉𝑖 𝑝𝑖

2𝑔 is the dynamic (or velocity), head. The summation of the static head and the elevation head, 𝛾 +𝑧𝑖 is referred to as the piezometric head.

The piezometric head is what is measured with the piezometer (manometer) board on the apparatus for this experiment.

Head loss, hL, includes the sum of pipe friction losses, hf and all minor losses.

ℎ𝐿 = ℎ𝑓 + ∑ ℎ𝑖

𝑖=1,2,…𝑛

where hi is the minor head loss (in meters) for the ith component and

n is the number of components (fittings, bends, etc.). Pipe friction losses are expressed as the Darcy

Wisbech equation given by

𝐿 𝑉2

ℎ𝑓 = 𝑓

𝐷2𝑔

where f is a friction factor, L is the pipe length, and x is the pipe diameter. Pipe friction losses are assumed to be negligible in this experiment. Minor losses occur at any bend, transition, or fitting where the streamlines are not straight and are proportional to the #velocity head. for all components, head loss is given by

𝑉2

ℎ𝑖 = 𝐾𝑖

2𝑔

where Ki is the loss coefficient (dimensionless) for the ith component and

V is the fluid velocity as it travels through the pipe component. For the expansion and contraction, the V used in the above equation hi is the velocity of the fluid in the smaller-diameter pipe.

**Apparatus:**

* Armfield Hydraulics Bench with Energy Losses apparatus
* Stopwatch

**Procedure**

**Observations:**

|  |  |  |  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- | --- |
| Sr# | Volume  (liter) | Time  (sec) | Flow rate  (m3/sec) | H1  (m) | H2  (m) | H3  (m) | H4  (m) | H5  (m) | H6  (m) | H7  (m) | H8  (m) |
| 1 |  |  |  |  |  |  |  |  |  |  |  |
| 2 |  |  |  |  |  |  |  |  |  |  |  |

**Calculations:**

|  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- |
| Sr.# | Flow  Rate  (m3/s) | Velocity in small pipe  (m/s) | Velocity  Head  (m) |  | Difference Piezometer Head | | |  |
| 90o  Elbow  (H1H2) | 45o  Elbow  (H3H4) | Sudden enlargement  (H5-H6) | Sudden contraction  (H6-H7) | 90O bend  (H7-H8) |
| 1 |  |  |  |  |  |  |  |  |
| 2 |  |  |  |  |  |  |  |  |

**Conclusion:**